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Cooling system design and humidity management

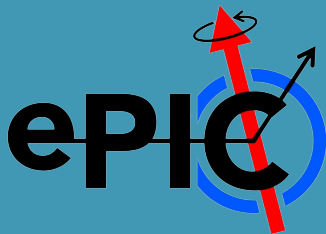
ePIC SVT Working Meeting at Oxford
2025-12-18

Joe Silber (LBNL) - mechanical engineer, presenting

Jaime Cruz Duran (LBNL) and Nick Payne (formerly LBNL) - CFD analyses

Nicole Apadula (LBNL) - thermal tests

Elaine Buron (LBNL) - CAD design



High level cooling requirements

From draft Preliminary Design Report (PDR):

| Table 9.2: SVT component temperature requirements (N/S is not specified). | | | | |
|---|-----|------------------------------------|-----|---------|
| Requirement | LEC | RSU | REC | AncASIC |
| Maximum T [°C] | 65 | 40 | N/S | 80 |
| Maximum T variation [°C] | 10 | 1 over 3 mm 10 over full length | N/S | 10 |

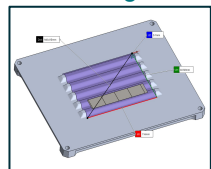
Design process from high level req'ts to detailed specs

High level requirements

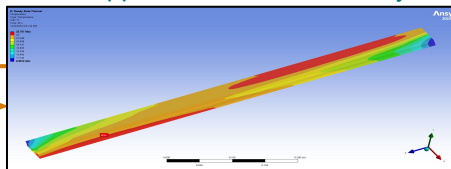
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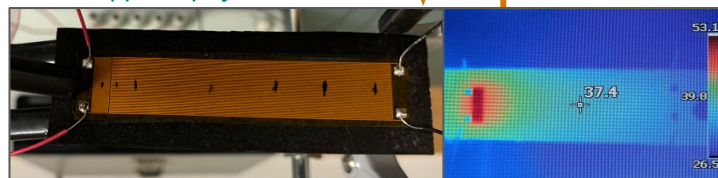
CAD design



Local supports heat transfer analysis



Local supports physical test



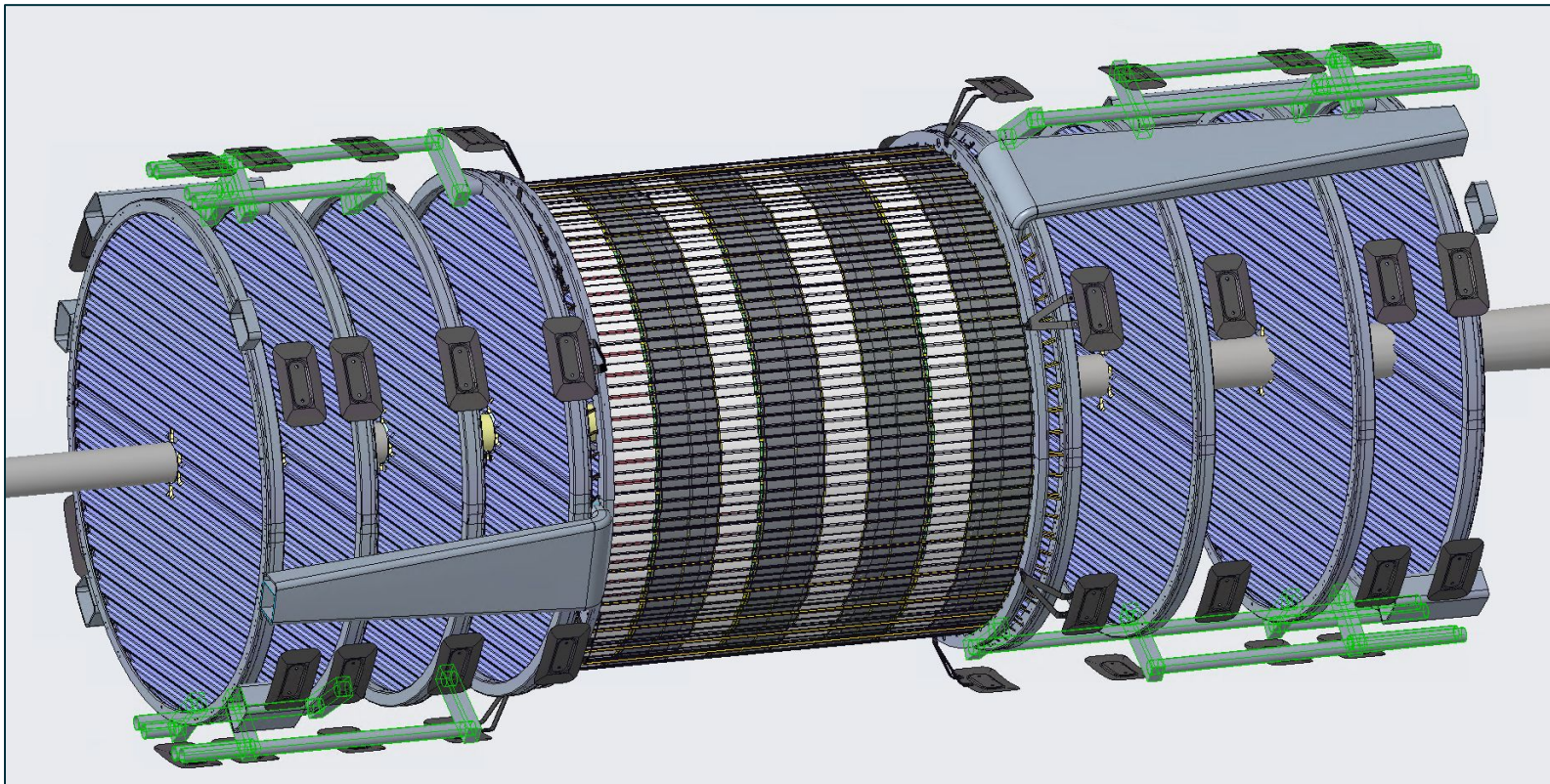
Req't on
 T_{max}

Constraints on
 ΔT , ΔP , air
speed

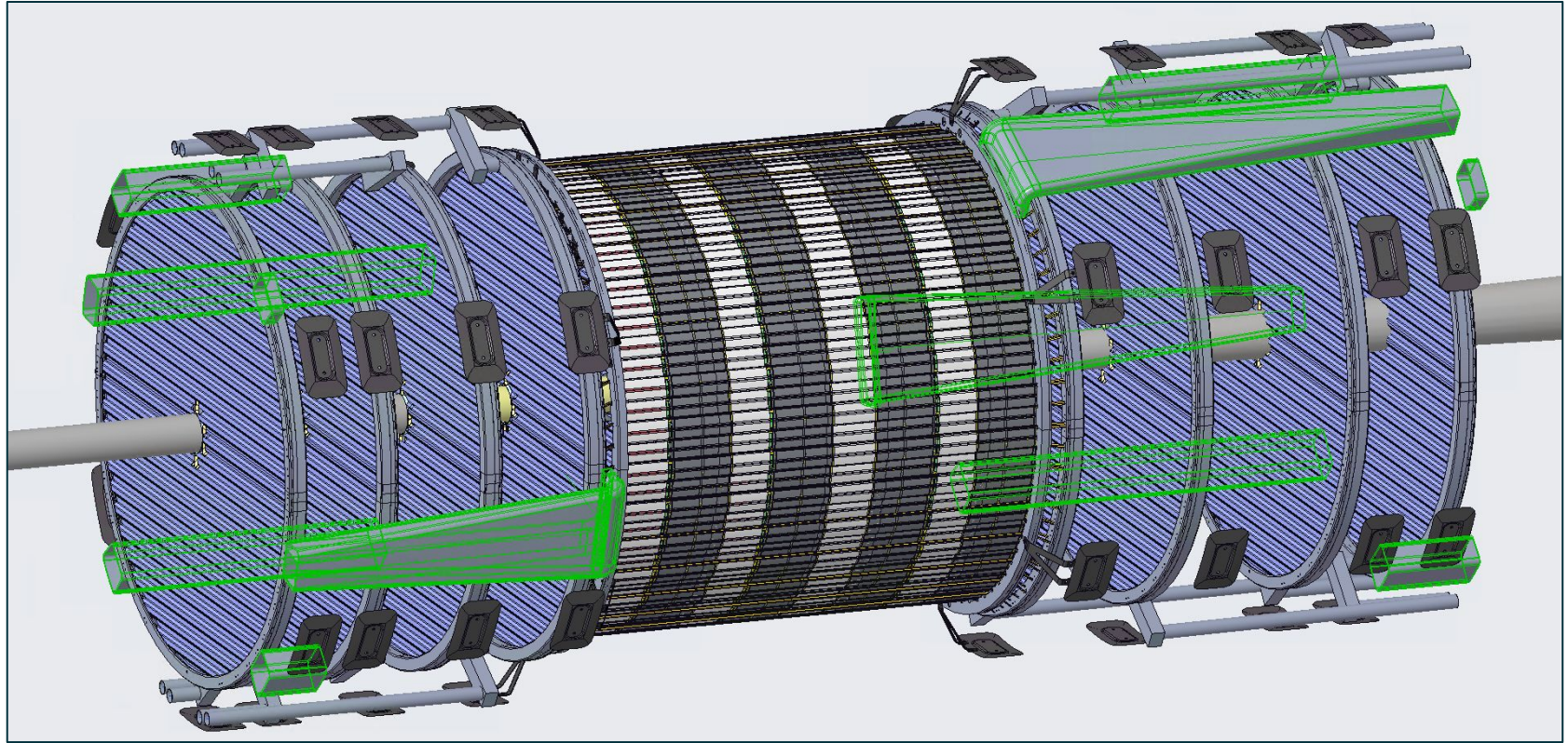
End-to-end system performance calculation

| | source → a16c | branches to hydrox + top + bottom halves | branches to hydrox + top half | branches to hydrox + bottom half | pipes into a16c to half disks and half halves | pipes within SVT to half disks and half halves | manifest | disk channels and valves | SVT internal valves | exhaust ducts | |
|---|------------------|---|--|--|--|---|----------|-----------------------------|------------------------|---------------|--------|
| stage description | - | - | - | - | - | - | - | - | - | - | |
| stage index | - | - | 0 | 1 | 2 | 3 | 4 | 5 | 6 | 7 | |
| num channels (per parent channel) | - | - | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 | |
| total num channels in system | - | - | N = product(n) | | | | | | | | 0.0160 |
| mass flow per channel | - | - | m = (n, or previous stage m) / n | | | | | | | | 12 |
| length | - | - | L = (m, or previous stage L) / n | | | | | | | | 0.0079 |
| hydraulic diameter (mm) | - | - | D_h = (m, or previous stage D_h) / n | | | | | | | | 0.0079 |
| hydraulic diameter | - | - | D_h = (m, or previous stage D_h) / n | | | | | | | | 0.0079 |
| single channel cross-sectional area along length L | - | - | A_s = π D ² / 4 | | | | | | | | 0.0079 |
| all channels total cross-sectional area | - | - | Σ A_s = A _{total} = N A_s | | | | | | | | 0.0079 |
| entrance temperature | - | - | T = T _{in} or previous stage T | | | | | | | | 0.0079 |
| entrance pressure | - | - | P = P _{in} or previous stage P | | | | | | | | 0.0079 |
| entrance density (ideal gas law) | - | - | ρ = P _{in} / (R T _{in}) | | | | | | | | 0.0079 |
| entrance dynamic viscosity | - | - | μ = μ(T _{in}) | | | | | | | | 0.0079 |
| Reynold's number | - | - | Re = 4 m / (π D _h μ) | | | | | | | | 0.0079 |
| friction factor (Blasius) | - | - | f = 0.316 / Re ^{0.25} otherwise | | | | | | | | 0.0079 |
| friction pressure drop (Darcy-Weisbach) | - | - | ΔP _f = f (L/D _h) (ρ v ² / 2) | | | | | | | | 0.0079 |
| downstream pressure | - | - | P _{out} = P _{in} - ΔP _f | | | | | | | | 0.0079 |
| ambient pressure in the downstream area of this stage | - | - | P _{amb} , ambient | | | | | | | | 0.0079 |
| downstream pressure relative to local ambient | - | - | description(P _{out} - P _{amb} , ambient) | | | | | | | | 0.0079 |
| module power input to stream | - | - | Q = C _p N (h _{out} - h _{in}) | | | | | | | | 0.0079 |

Air supply pipes



Air exhaust ducts



ePIC SVT - cooling system diagram

| Rev | Date | Author | Description |
|-----|------------|-------------------|----------------------------------|
| v1 | 2025-12-11 | Joe Silber (LBNL) | initial release |
| v2 | 2025-12-12 | Joe Silber (LBNL) | add liquid system |
| v3 | 2025-12-16 | Joe Silber (LBNL) | space out e-/hadron & top/bottom |
| | | | |
| | | | |
| | | | |

Nomenclature

SVT ... Silicon Vertex Tracker
TBD ... To Be Determined
L# ... Barrel layer IDs
D# ... Disk IDs
V# ... Disk interstitial volume IDs
LV# ... Barrel layer interstitial volume IDs
SCB ... Segment Control Board
CB ... Control Board

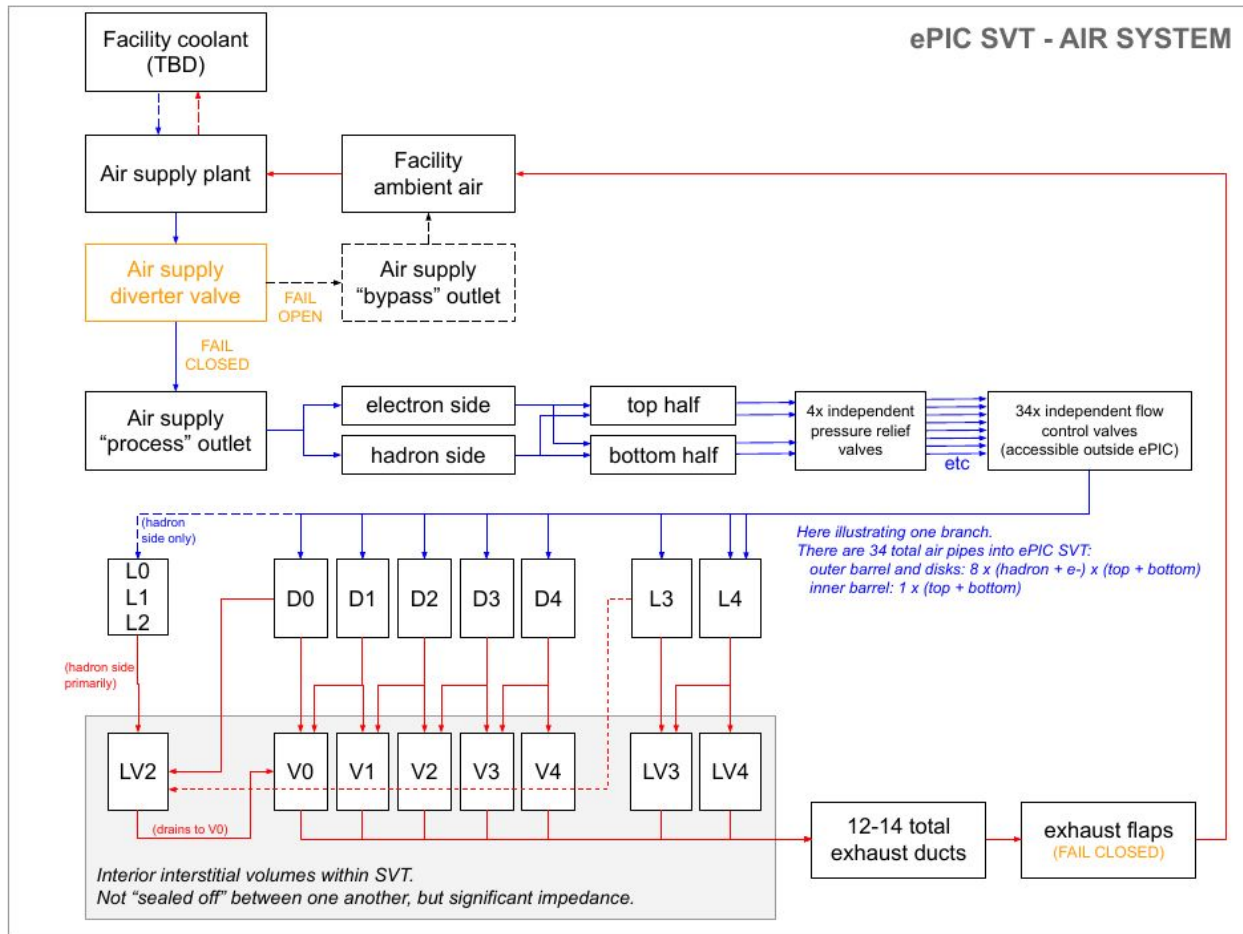
Notes

1. Graphical elements not intended to follow any standard.
2. Color-coding consistency not guaranteed.

Link:

[ePIC SVT cooling system diagram - v3.pdf](#)

ePIC SVT - AIR SYSTEM



Air exhaust

- Exhaust via 12-14 ducts
- Duct hydraulic $\varnothing 62$ mm
 - I.e. much greater cross-section than input pipes (4 x $\varnothing 50$ mm)
- Ducts draw from interior volumes (see diagram)
- These volumes aren't "sealed" from each other, but significant impedance
- Suction could be done but probably not necessary
- Flapper valves at outlets to prevent ingress when flow off

ePIC SVT - interior air volumes diagram

| Rev | Date | Author | Description |
|-----|------------|-------------------|-----------------|
| v1 | 2025-12-11 | Joe Silber (LBNL) | initial release |
| | | | |
| | | | |
| | | | |

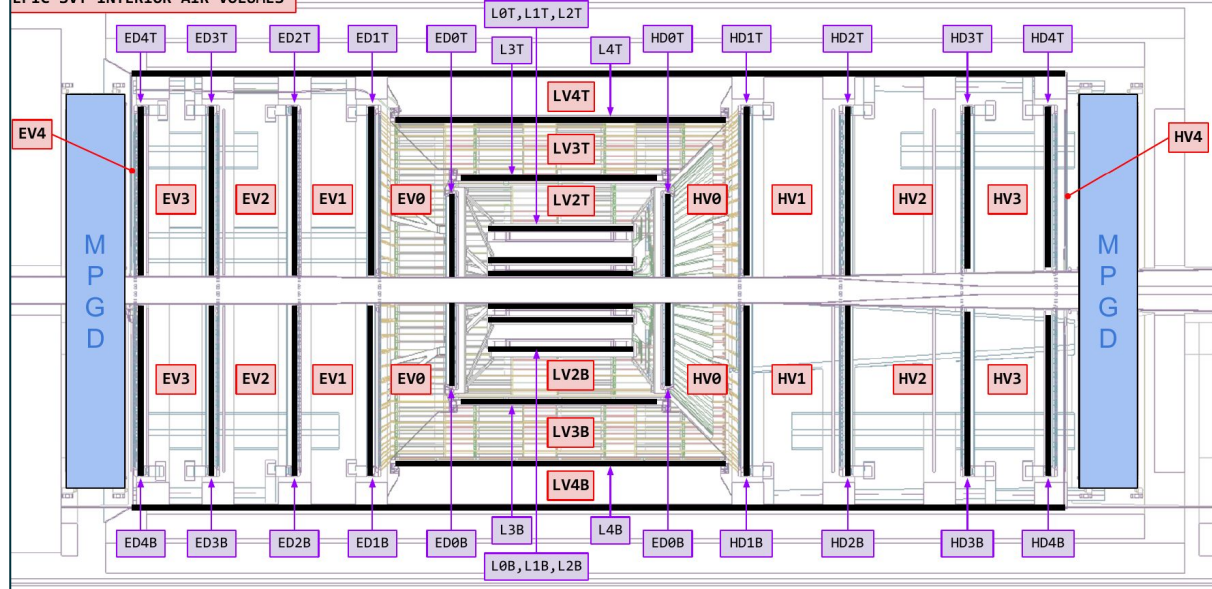
Notes

1.

References

1. [Live editable version of this document](#)
2. [ePIC SVT cooling system diagram](#)
3. [ePIC SVT cooling air flow stages](#)

EPIC SVT INTERIOR AIR VOLUMES



Link: [ePIC SVT interior air volumes diagram - v1.pdf](#)


System calculator inputs: local supports geometry

| | A | B | C | D | E | F | G | |
|----|--|--|-----|-------|---|---|---|--|
| 51 | Disk geometry | | | | | | | |
| 52 | corrugation pitch | xc | mm | 34.7 | | | | |
| 53 | corrugation height | hc | mm | 6 | | | | |
| 54 | corrugation cross-sectional area | Ac ~ xc * hc / 2 | mm² | 104.1 | | | | |
| 55 | corrugation hydraulic diameter | Dc = √(4 Ac / π) | mm | 11.5 | | | | |
| 56 | large disk diameter (D1-D4) | Dd14 | mm | 870 | | | | |
| 57 | small disk diameter (D0) | Dd0 | mm | 488 | | | | |
| 58 | num large disks (per side) | nd14 | - | 4 | | | | |
| 59 | num small disks (per side) | nd0 | - | 1 | | | | |
| 60 | avg disk diameter (areally weighted) | Dd = √((Dd14²*nd14+Dd0²*nd0)/(nd14+nd0)) | mm | 808.2 | | | | |
| 61 | avg large disk corrugation length | Lc14 ~ π / 4 * Dd14 | mm | 683.3 | | | | |
| 62 | avg small disk corrugation length | Lc0 ~ π / 4 * Dd0 | mm | 383.3 | | | | |
| 63 | avg corrugation length | Lc ~ π / 4 * Dd | mm | 634.7 | | | | |
| 64 | avg num corrugations (per half disk) | ncd ~ (Dd/2) / (xc/2) | - | 23.3 | <-- non-integer is ok, it's averaging large and small disks | | | |
| 65 | | | | | | | | |
| 66 | Layers geometry | | | | | | | |
| 67 | stave channel width (this is one side) | ws | mm | 20.65 | | | | |
| 68 | stave channel height at edge | hs1 | mm | 2.92 | | | | |
| 69 | stave channel height at center | hs2 | mm | 7.49 | | | | |
| 70 | stave channel avg height | hs = (hs1 + hs2)/2 | mm | 5.2 | | | | |
| 71 | stave channel cross-sectional area | As ~ ws * hs | mm² | 107.5 | | | | |
| 72 | stave channel hydraulic diameter | Ds = √(4 As / π) | mm | 11.7 | | | | |
| 73 | variation from disk corrug hydraulic diameter | Ds / Dc - 1 | - | 1.6% | <-- this is pretty similar to disk corrugation hydraulic diameter | | | |
| 74 | L4 stave length | Ls4 | mm | 793 | | | | |
| 75 | L3 stave length | Ls3 | mm | 503 | | | | |
| 76 | num L4 staves (per top/bottom half) | ns4 | - | 35 | | | | |
| 77 | num L3 staves (per top/bottom half) | ns3 | - | 22 | | | | |
| 78 | avg stave channel length | Ls = (Ls4*ns4+Ls3*ns3)/(ns4+ns3) | mm | 681.1 | | | | |
| 79 | variation from disk corrug avg length | Ls / Lc - 1 | - | 7.3% | <-- this is pretty similar to disk average corrugation length | | | |
| 80 | Note: given geometric similarity of average barrel staves to average disk corrugation channels, I treat them all as basically the same in flow calcs below. | | | | | | | |
| 81 | num half disks equivalent to an OB half | nds_equiv = Ls * (ns4 + ns3) / (Lc * nc) | | 2.6 | <-- non-integer is ok, it's averaging lots of things | | | |
| 82 | | | | | | | | |

System calculator inputs: internal volumes and exhaust

| | A | B | C | D |
|-----|--|--|-----------------|----------|
| 89 | SVT internal volume geometry | | | |
| 90 | approx percent of internal volume which is ambient air | v_{f_amb} | - | 90% |
| 91 | PST diameter | D_{pst} | mm | 1076 |
| 92 | PST length | L_{pst} | mm | 2540 |
| 93 | SVT total internal ambient air volume | $v_{svt} = v_{f_amb} * \pi/4 * D_{pst}^2 * L_{pst}$ | mm ³ | 2.08E+09 |
| 94 | number of internal ambient air subvolumes | n_v | - | 12 |
| 95 | average SVT internal subvolume's volume | $v_{va} = v_{svt} / n_v$ | mm ³ | 1.73E+08 |
| 96 | num subvolumes between large disks | n_{vl} | - | 6 |
| 97 | typical gap between large disks | g_{vl} | mm | 423.2 |
| 98 | rough equiv hydraulic diameter between large disks | $D_{vl} = \sqrt{4 / \pi * D_{pst} * g_{vl}}$ | mm | 761.4 |
| 99 | L4 diameter | D_{L4} | mm | 840 |
| 100 | L3 diameter | D_{L3} | mm | 540 |
| 101 | rough equiv hydraulic diameter outside L4 | $Dh_{L4} = \sqrt{D_{pst}^2 - D_{L4}^2}$ | mm | 672.4 |
| 102 | rough equiv hydraulic diameter between L3/L4 | $Dh_{L34} = \sqrt{D_{L4}^2 - D_{L3}^2}$ | mm | 643.4 |
| 103 | average SVT internal subvolume's hydraulic diameter | $D_{va} = (n_{vl} * D_{vl} + D_{L3} + Dh_{L34} + Dh_{L4}) / (n_v)$ | mm | 713.8 |
| 104 | average SVT internal subvolume's length | $L_{va} = v_{va} / (\pi/4 * D_{va}^2)$ | mm | 432.8 |
| 105 | | | | |
| 106 | Exhaust duct geometry | | | |
| 107 | exhaust duct width | w_{ex} | mm | 55 |
| 108 | exhaust duct height | h_{ex} | mm | 70 |
| 109 | exhaust duct cross-sectional area | $A_{ex} = w_{ex} * h_{ex}$ | mm ² | 3850 |
| 110 | exhaust duct perimeter | $P_{ex} = 2 * (w_{ex} + h_{ex})$ | mm | 250 |
| 111 | exhaust duct hydraulic diameter | $D_{ex} = 4 A_{ex} / P_{ex}$ | mm | 61.6 |
| 112 | number of exhaust ducts per internal ambient subvolume | n_{ex} | - | 1 |

System calculator inputs: module power loads

| | A | B | C | D | E | F | G |
|-----|--|--|--|--------|---|---|---|
| 114 | Module power loads | | | | | | |
| 115 | reference link for power loads |  Copy of EIC-LAS Power - 2025-10-22 | Also see adjoining sheet where RSUs are counted in an alternate way. | | | | |
| 116 | power per LEC | Q_1lec | W | 0.208 | | | |
| 117 | power per RSU | Q_1rsu | W | 0.208 | | | |
| 118 | typical num RSU per module | n_rsu_per_mod | - | 5.652 | <-- average, calculated on adjoining sheet | | |
| 119 | typical EIC-LAS power | $Q_{eiclas} = n_{rsu_per_mod} * Q_{1rsu} + Q_{1lec}$ | W | 1.38 | | | |
| 120 | AncASIC power multiple of EIC-LAS | qf_aa | - | 45% | | | |
| 121 | typical power per AncASIC | $Q_{1aa} = qf_aa * Q_{eiclas}$ | W | 0.62 | | | |
| 122 | FPC power multiple of EIC-LAS | qf_fpc | - | 30% | | | |
| 123 | typical power per FPC | $Q_{1fpc} = qf_fpc * Q_{eiclas}$ | W | 0.42 | | | |
| 124 | length per RSU | L_rsu | mm | 21.6 | | | |
| 125 | num rsu per avg corrug length (exact coverage) | $n_{rsu} = L_c / L_{rsu}$ | - | 29.4 | <-- non-integer is ok, it's averaging stuff | | |
| 126 | num modules per avg corrug length | $n_{mod} = n_{rsu} / n_{rsu_per_mod}$ | - | 5.2 | | | |
| 127 | total RSU power per avg corrug | $Qc_rsu = Q_{1rsu} * n_{rsu}$ | W | 6.11 | | | |
| 128 | total LEC power per avg corrug | $Qc_lec = Q_{1lec} * n_{mod}$ | W | 1.08 | | | |
| 129 | total AncASIC power per avg corrug | $Qc_aa = Q_{1aa} * n_{mod}$ | W | 3.24 | | | |
| 130 | total FPC power per avg corrug | $Qc_fpc = Q_{1fpc} * n_{mod}$ | W | 2.16 | | | |
| 131 | total power per avg corrug | $Qc = Qc_rsu + Qc_lec + Qc_aa + Qc_fpc$ | W | 12.59 | | | |
| 132 | total power per avg module | $Q_{mod} = Qc / n_{mod}$ | W | 2.42 | <-- cross-check this against others' current-best-estimates | | |
| 133 | total modules modeled below | $n_{mod_system} = L_4 * N_4 * n_{mod}$ | - | 3693.8 | <-- cross-check this against others' current-best-estimates | | |

System calculator inputs: boundary conditions

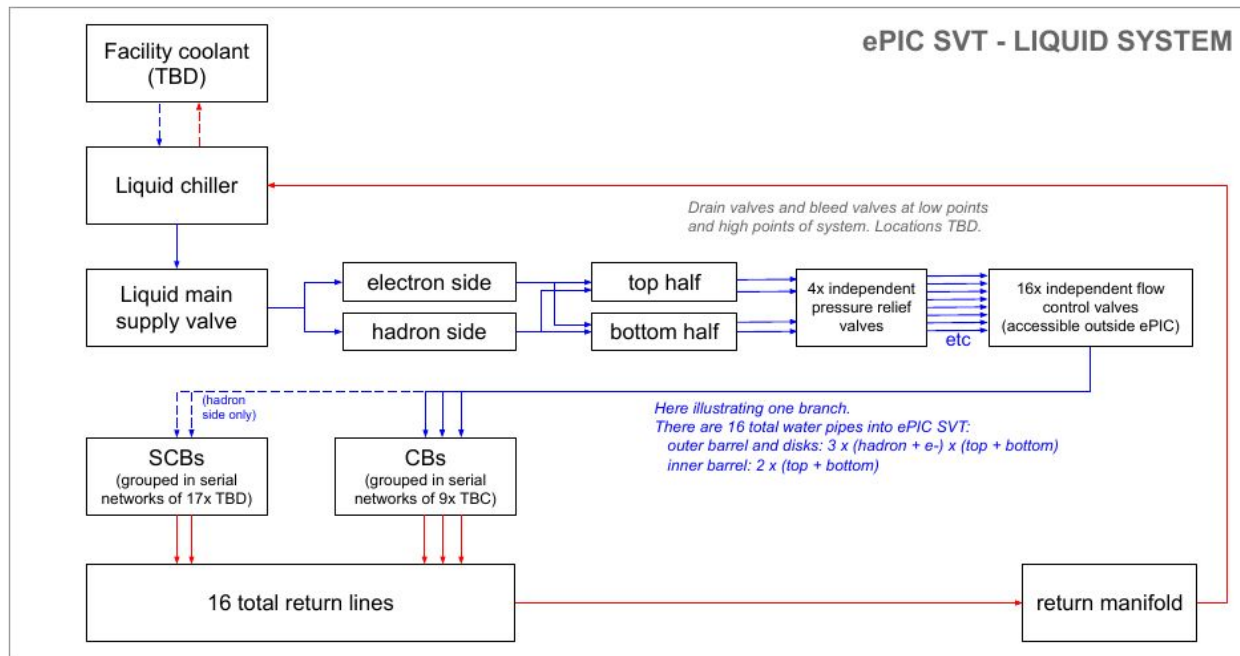
| | A | B | C | D | E | F | G |
|-----|---|--------------|-----------------------------|---------|---|---|--------------------|
| 135 | Boundary conditions | | | | | | |
| 136 | source temperature | T_s | °C | 2.8 | 276.0 K | | |
| 137 | source pressure | P_s | bar | 1.427 | 0.413 bar (gauge) | | Iteratively solved |
| 138 | " | " | Pa | 142,654 | 41,329 Pa (gauge) | | |
| 139 | " | " | psi | 20.7 | 6.0 psi (gauge) | | |
| 140 | source mass flow rate | \dot{m}_s | kg/s | 0.95 | | | |
| 141 | SVT internal ambient volume's positive pressurization | ΔP_+ | bar (gauge) | 0.03 | must be ≥ 0 | | |
| 142 | " | " | in H ₂ O (gauge) | 12.0 | | | |
| 143 | SVT internal ambient volume's pressure | P_β | bar | 1.043 | must be ≥ 1.01325 (external atmospheric) | | |
| 144 | " | " | atm | 1.030 | | | |

Cooling system performance baseline

- source temperature = 2.8°C
- total mass flow = 0.95 kg/s
- total volume flow = 1135 cfm @ source pressure, 1604 cfm @ exhaust
- source pressure = 1.43 bar → 1.03 bar positive pressure @ exhaust
- channel/stave entrance temperature = 5.0°C
- channel/stave air speed = 10.0 m/s
- total power extracted = 8.9 kW
- SVT internal ambient temperature = 14.4°C

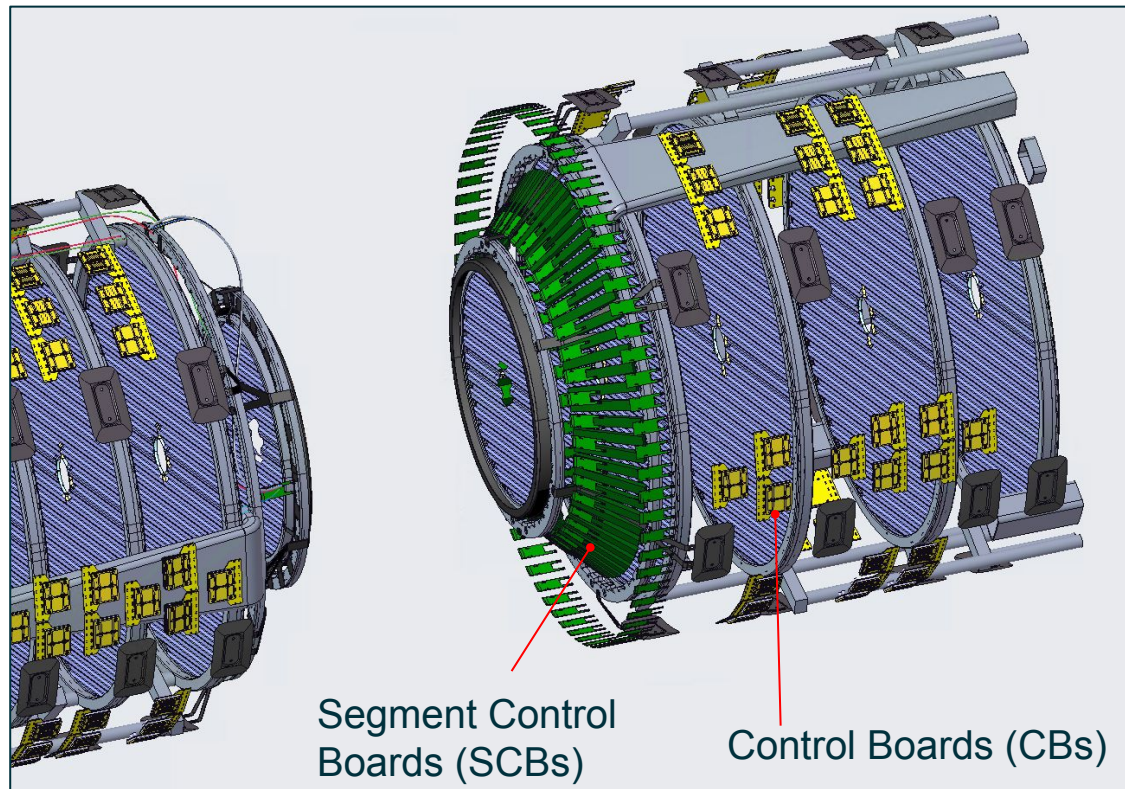
| | A | B | C | D | E | F | G | H | I | J | K | L |
|-----|---|---|-------------------|---------------|-------------------------------------|---------------------------------|--|---|----------------|--------------------------|------------------------------|---------------|
| | source → manifold → inter area change | | | source → ePIC | branches to hadron + electron sides | branches to top + bottom halves | pipes into ePIC to half disks and half barrels | pipes within SVT to half disks and half barrels | manifold | disk channels and staves | SVT internal ambient volumes | exhaust ducts |
| 150 | stage description | - | - | 0 | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 |
| 151 | stage index | - | - | 1 | 2 | 2 | 8 | 1 | 1 | 22.2 | 0.0169 | 1 |
| 152 | num channels (per parent channel) | $N_i = \text{product}(n_i)$ | m | 1 | 2 | 4 | 32 | 32 | 32 | 710 | 12 | 12 |
| 153 | total num channels in system | $\dot{m} = (\dot{m}_s \text{ or previous stage } \dot{m}) / n_i$ | kg/s | 0.950 | 0.475 | 0.238 | 0.030 | 0.030 | 0.030 | 0.001 | 0.079 | 0.079 |
| 154 | mass flow per channel | L | m | 10.000 | 10.000 | 15.000 | 7.000 | 3.000 | 0.100 | 0.635 | 0.433 | 10.000 |
| 155 | length | D_mm | mm | 100 | 75 | 50 | 23 | 23 | 23 | 11.5 | 713.8 | 61.6 |
| 156 | hydraulic diameter (mm) | $A_{12} = \pi D^2 / 4$ | m ² | 7.85E-03 | 4.42E-03 | 1.96E-03 | 4.15E-04 | 4.15E-04 | 4.15E-04 | 1.04E-04 | 4.00E-01 | 2.98E-03 |
| 157 | single channel cross-sectional area along length L | $\Sigma A_{12} = A_{12,i} * N_i$ | cm ² | 78.5 | 88.4 | 78.5 | 133.0 | 133.0 | 133.0 | 739.6 | 48,024.7 | 357.6 |
| 160 | all channels total cross-sectional area | $T_1 = T_s \text{ or previous stage } T_s$ | °C | 2.8 | 3.2 | 2.4 | 3.9 | 3.7 | 3.5 | 5.0 | 14.4 | 14.2 |
| 162 | entrance temperature | $P_1 = P_s \text{ or previous stage } P_s$ | bar | 1.427 | 1.390 | 1.325 | 1.178 | 1.084 | 1.040 | 1.044 | 1.043 | 1.039 |
| 164 | entrance pressure | $Re = 4 \dot{m} / (\pi D \mu_i)$ | - | 6.99E+05 | 4.66E+05 | 3.50E+05 | 9.48E+04 | 9.48E+04 | 9.48E+04 | 8.50E+03 | 7.91E+03 | 9.18E+04 |
| 167 | Reynold's number | $\Delta P_{12} = -f * (L/D) * \dot{m}^2 / (2 \rho_1 A_{12}^2)$ | Pa | -4,438 | -5,317 | -17,025 | -9,440 | -4,394 | -153 | -114 | 0 | -825 |
| 169 | friction pressure drop (Darcy-Weisbach) | $P_2 = P_1 + \Delta P_{12}$ | bar | 1.382 | 1.337 | 1.154 | 1.084 | 1.040 | 1.039 | 1.043 | 1.043 | 1.031 |
| 171 | downstream pressure | $P_{\text{local_ambient}}$ | bar | 1.013 | 1.013 | 1.013 | 1.043 | 1.043 | 1.043 | 1.043 | 1.043 | 1.013 |
| 172 | ambient pressure in the downstream area of this stage | description($P_2 - P_{\text{local_ambient}}$) | - | positive | positive | positive | positive | approx neutral | approx neutral | approx neutral | approx neutral | positive |
| 173 | downstream pressure relative to local ambient | $Q = Q_c * N_i \text{ if channel or stave else } 0$ | W | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 8943.9 | 0.0 | 0.0 |
| 174 | module power input to stream | $\Delta T_{q12} = Q / (N_i * \dot{m} * c_p)$ | K | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 9.4 | 0.0 | 0.0 |
| 175 | stream temperature rise due to external heat input | $T_2 = T_1 + \Delta T_{q12} + \Delta T_{k12}$ | °C | 2.7 | 3.0 | 1.6 | 3.7 | 3.5 | 3.5 | 14.3 | 14.4 | 14.2 |
| 181 | downstream temperature | $V_a = \dot{m} / \rho_a$ | m ³ /s | 0.536 | 0.276 | 0.151 | 0.021 | 0.022 | 0.023 | 0.001 | 0.063 | 0.063 |
| 185 | average volumetric flow | $\Sigma V_a = V_a * N_i$ | m ³ /s | 0.536 | 0.552 | 0.605 | 0.667 | 0.710 | 0.726 | 0.738 | 0.751 | 0.757 |
| 187 | total volumetric flow (all channels) | " | cfm | 1134.9 | 1170.2 | 1282.8 | 1414.1 | 1505.3 | 1537.9 | 1564.8 | 1592.3 | 1603.5 |
| 188 | " | $u_a = V_a / A_{12}$ | m/s | 68.2 | 62.5 | 77.1 | 50.2 | 53.4 | 54.6 | 10.0 | 0.2 | 21.2 |
| 189 | average air speed | $\beta_{3n} = P_{3n} / P_2$ | - | 1.006 | 0.993 | 1.028 | 1.000 | 1.000 | 1.018 | 1.001 | 0.997 | 1.003 |
| 194 | pressure ratio calculated with non-choked eqn | $\beta_{3n} < \beta_x$ | boolean | FALSE | FALSE | FALSE | FALSE | FALSE | FALSE | FALSE | FALSE | FALSE |
| 195 | is choked? | $\dot{E}_{\text{err}} = (\dot{E}_2 - \Sigma Q_i) - \dot{E}_{1_stage0}$ | W | -2 | -4 | -24 | -26 | -27 | -27 | -24 | -24 | -24 |
| 214 | system energy balance error | $\dot{E}_{\text{err_frac}} = \dot{E}_{\text{err}} / \dot{E}_{1_stage0}$ | - | -0.001% | -0.002% | -0.009% | -0.010% | -0.010% | -0.010% | -0.009% | -0.009% | -0.009% |
| 215 | system energy balance error fraction (w.r.t. total energy) | $\dot{E}_{\text{err_frac}} = \dot{E}_{\text{err}} / \Sigma Q_i$ | - | -0.027% | -0.049% | -0.274% | -0.293% | -0.307% | -0.307% | -0.272% | -0.272% | -0.272% |
| 216 | system energy balance error fraction (w.r.t. total input power) | | | | | | | | | | | |

Link: [ePIC SVT cooling air flow stages - v15.xlsx](#)



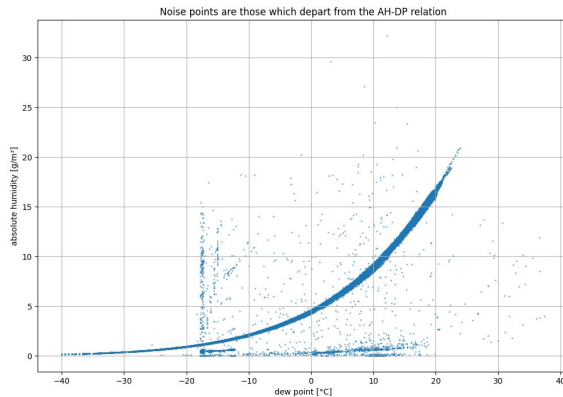
Liquid cooling of CBs and SCBs

- Current thought is to group CBs into serial cooling chains of ~9x
 - i.e. 12x such networks
 - assemble and test a network outside detector, prior to assembly
 - still working on patterning
 - might make sense to unify multiple CBs into fewer cold plates
- And group SCBs into networks of 17x
- Very much a work in progress

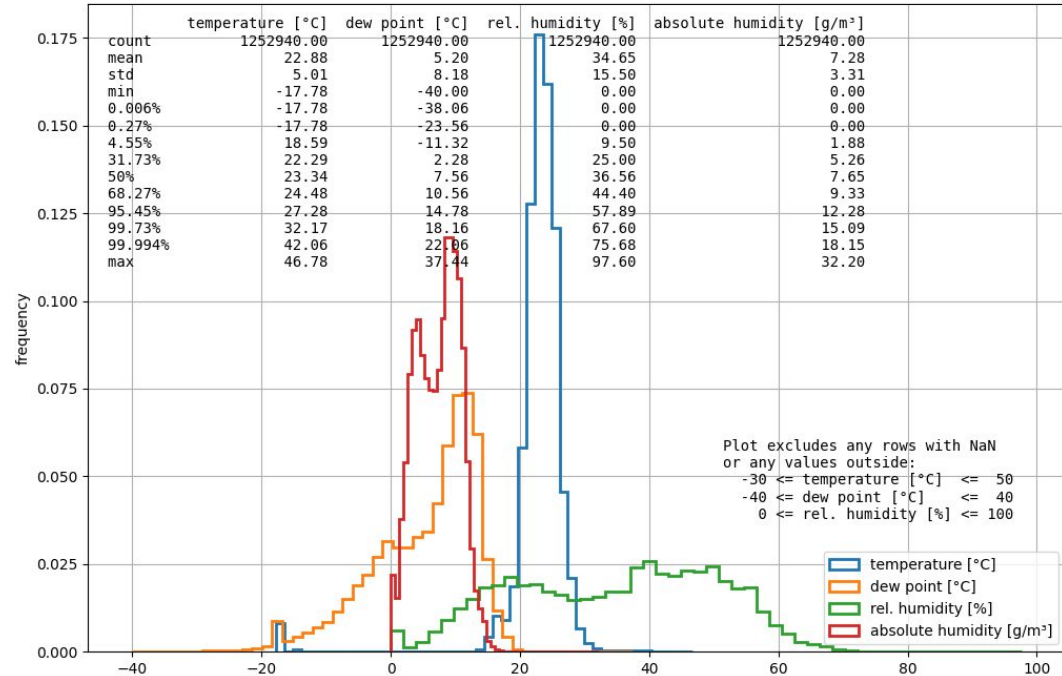


STAR WAH environmental data over 14 years

- extreme hot/wet condition:
 - dew point ~ 22.1 C
 - ambient temp ~ 35.0 C
- Some noise in the WAH data
- Especially early in time history
- But I'm pretty confident the hot/wet condition stated above was a real event – see abs humidity vs dew point (these are physically correlated)



STAR Wide Angle Hall weather data
2010-12-07 to 2025-01-07



System calculator inputs: humidity and insulation

| | A | B | C | D | E |
|----|--|---|-----------------|---------|---|
| 39 | Insulation properties, boundary conditions, and assumptions | | | | |
| 40 | insulation material thermal conductivity | k_insul | W/(m*K) | 0.02 | <-- 0.05 for typical insulation wraps, ATLAS uses silica aerogel ~ 0.02 W/(m*K) |
| 41 | " | " | US R-value @ 1" | 7.2 | |
| 42 | insulation thickness design factor | t_design_factor | - | 2.0 | |
| 43 | typical convection coefficient outside insulation | h_insul | W/(m² * K) | 5.0 | |
| 44 | exterior hot/wet dew point | Td_humid | °C | 22.1 | 4σ (99.994% envelope) value in WAH data 2010-2025 |
| 45 | exterior hot/wet temperature | Tamb_humid | °C | 35.0 | corresponding ambient temperature in WAH data 2010-2025 |
| 46 | SVT interior average air temperature | Tamb_svt | °C | 14.4 | from calculations below |
| 47 | air supply relative humidity | RH_supply | % | 30% | |
| 48 | SVT interior dewpoint calc intermediate term | $y_svt = \ln(RH_supply * \exp((17.62 * T_amb_svt) / (243.12 + T_amb_svt)))$ | - | -0.2192 | using Magnus model |
| 49 | SVT interior dew point | $Td_svt = (243.12 * y) / (17.62 - y)$ | °C | -3.0 | assuming 100% displacement of by supply (i.e. supply input >> moist air back flow or effusion from outside ambient) |

↑
This assumed -3°C dew point value is used to size the insulation (next slide). It assumes an HVAC-like supply (30% RH). I expect it will end up being quite conservative because we more likely will buy a compressed air system with Class 2 (-40°C) or Class 3 (-20°C) pressure dew point.

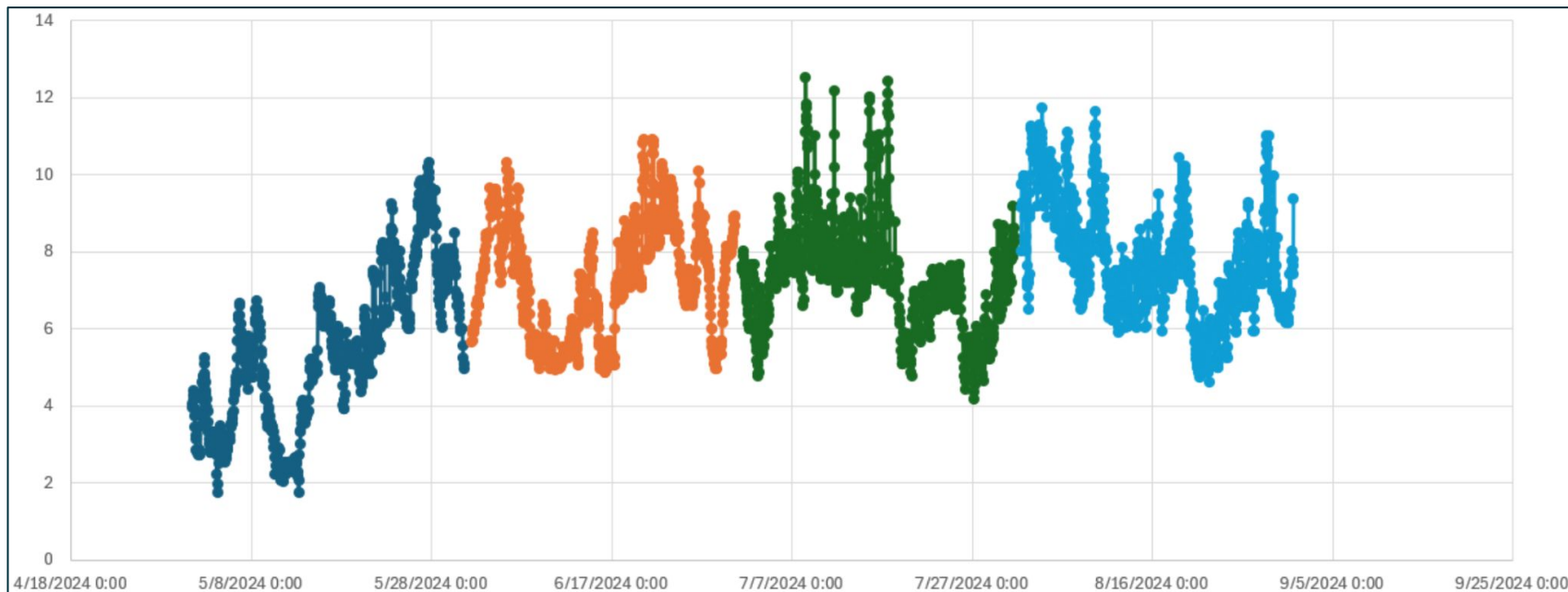
Baseline calculations of insulation thickness

| | A | B | C | D | E | F | G | H | I | J | K | L |
|-----|---|--|---------|-------------------|---|---------------------------------------|--|--|----------|-----------------------------|------------------------------------|---------------|
| | stage description | | | source -> ePIC | branches to hadron + electron sides | branches to top + bottom halves | pipes into ePIC to half disks and half barrels | pipes within SVT to half disks and half barrels | manifold | disk channels and staves | SVT internal ambient volumes | exhaust ducts |
| 150 | stage description | - | - | 0 | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 |
| 151 | stage index | - | - | 1 | 2 | 2 | 8 | 1 | 1 | 22.2 | 0.0169 | 1 |
| 152 | num channels (per parent channel) | n_i | - | 1 | 2 | 4 | 32 | 32 | 32 | 710 | 12 | 12 |
| 153 | total num channels in system | $N_i = \text{product}(n_i)$ | m | 0.950 | 0.475 | 0.238 | 0.030 | 0.030 | 0.030 | 0.001 | 0.079 | 0.079 |
| 154 | mass flow per channel | $\dot{m} = (\dot{m}_s \text{ or previous stage } \dot{m}) / n_i$ | kg/s | 10.000 | 10.000 | 15.000 | 7.000 | 3.000 | 0.100 | 0.635 | 0.433 | 10.000 |
| 155 | length | L | m | 100 | 75 | 50 | 23 | 23 | 23 | 11.5 | 713.8 | 61.6 |
| 156 | hydraulic diameter (mm) | D_mm | mm | 1 | 1 | 1 | 1 | 0 | 0 | 0 | n/a | 1 |
| 219 | is exterior? (fully or partially) | - | boolean | 2.7 | 3.0 | 1.6 | 3.7 | 3.5 | 3.5 | 5.0 | - | 14.2 |
| 221 | min temperature this stage | $T_{min} = \min(T_1, T_2)$ | °C | -19.4 | -19.1 | -20.5 | -18.4 | 6.5 | 6.5 | 8.0 | - | -7.9 |
| 222 | air stream temperature relative to the local dewpoint | $\Delta T_d = T_{min} - \text{select}(T_d)$ | °C | 19.4 | 19.1 | 20.5 | 18.4 | 0.0 | 0.0 | 0.0 | - | 7.9 |
| 223 | temperature difference needing insulation | $\Delta T_{insul} = \text{abs}(\min(0, \Delta T_{insul}))$ | °C | 12.9 | 12.9 | 12.9 | 12.9 | 17.4 | 17.4 | 17.4 | - | 12.9 |
| 224 | temperature diff from a condensing surface to local ambient | $\Delta T_{cond2amb} = \text{select}(T_{amb}) - \text{select}(T_d)$ | °C | 6.0 | 5.9 | 6.4 | 5.7 | 0.0 | 0.0 | 0.0 | - | 2.5 |
| 225 | iterative thickness calc intermediate value | $\lambda = k * \Delta T_{insul} / (h_{insul} * \Delta T_{cond2amb})$ | mm | 111.4 | 86.1 | 61.5 | 32.7 | 23.0 | 23.0 | 11.5 | - | 66.3 |
| 226 | insulation minimum outside diameter (neglects pipe wall) | $D_{min_insul} = 2 * \lambda / \ln(D_{insul} / D)$ | mm | 5.7 | 5.5 | 5.7 | 4.8 | 0.0 | 0.0 | 0.0 | - | 2.4 |
| 227 | insulation minimum thickness (no margin) | t_min_insul | mm | 11.4 | 11.1 | 11.5 | 9.7 | 0.0 | 0.0 | 0.0 | - | 4.7 |
| 228 | insulation design thickness | t_insul = t_design_factor * t_min_insul | mm | 122.9 | 97.1 | 72.9 | 42.3 | 23.0 | 23.0 | 11.5 | - | 71.1 |
| 229 | pipe + insulation outer diameter (pipe wall neglected) | D_total_no_wall | mm | | | | | | | | | |

With respect to either the exterior extreme dew point value (22.1°C) or the interior (-3°C).

This 10 mm thick insulation around the hydraulic Ø23 mm air pipes occurs in the region of uncertain dryness within ePIC but outside SVT. May be challenging to cross-sectional area.

sPHENIX Hall (IR) dewpoint data May-Aug 2024



(courtesy Dan Cacace)

Same insulation calcs as before, but assuming:

1. max exterior dew point in the Wide Angle Hall is 13°C rather than 22.1°C
2. interlock stops operation when DP > 13°C (i.e. WAH HVAC goes down)

| | A | B | C | D | E | F | G | H | I | J | K | L |
|-----|---|---|---------|-------------------|---|---------------------------------------|--|--|----------|-----------------------------|------------------------------------|---------------|
| | stage description | | | source -> ePIC | branches to hadron + electron sides | branches to top + bottom halves | pipes into ePIC to half disks and half barrels | pipes within SVT to half disks and half barrels | manifold | disk channels and staves | SVT internal ambient volumes | exhaust ducts |
| 150 | stage index | - | - | 0 | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 |
| 151 | num channels (per parent channel) | n_i | - | 1 | 2 | 2 | 8 | 1 | 1 | 22.2 | 0.0169 | 1 |
| 152 | total num channels in system | $N_i = \text{product}(n_i)$ | m | 1 | 2 | 4 | 32 | 32 | 32 | 710 | 12 | 12 |
| 153 | mass flow per channel | $\dot{m} = (\dot{m}_i \text{ or previous stage } \dot{m}) / n_i$ | kg/s | 0.950 | 0.475 | 0.238 | 0.030 | 0.030 | 0.030 | 0.001 | 0.079 | 0.079 |
| 154 | length | L | m | 10.000 | 10.000 | 15.000 | 7.000 | 3.000 | 0.100 | 0.635 | 0.433 | 10.000 |
| 155 | hydraulic diameter (mm) | D_mm | mm | 100 | 75 | 50 | 23 | 23 | 23 | 11.5 | 713.8 | 61.6 |
| 156 | is exterior? (fully or partially) | - | boolean | 1 | 1 | 1 | 1 | 0 | 0 | 0 | n/a | 1 |
| 219 | min temperature this stage | $T_{\min} = \min(T_1, T_2)$ | °C | 2.7 | 3.0 | 1.6 | 3.7 | 3.5 | 3.5 | 5.0 | - | 14.2 |
| 221 | air stream temperature relative to the local dewpoint | $\Delta T_d = T_{\min} - \text{select}(T_d)$ | °C | -10.3 | -10.0 | -11.4 | -9.3 | 6.5 | 6.5 | 8.0 | - | 1.2 |
| 222 | temperature difference needing insulation | $\Delta T_{\text{insul}} = \text{abs}(\min(0, \Delta T_{\text{insul}}))$ | °C | 10.3 | 10.0 | 11.4 | 9.3 | 0.0 | 0.0 | 0.0 | - | 0.0 |
| 223 | temperature diff from a condensating surface to local ambient | $\Delta T_{\text{cond2amb}} = \text{select}(T_{\text{amb}}) - \text{select}(T_d)$ | °C | 22.0 | 22.0 | 22.0 | 22.0 | 17.4 | 17.4 | 17.4 | - | 22.0 |
| 224 | iterative thickness calc intermediate value | $\lambda = k * \Delta T_{\text{insul}} / (h_{\text{insul}} * \Delta T_{\text{cond2amb}})$ | mm | 1.9 | 1.8 | 2.1 | 1.7 | 0.0 | 0.0 | 0.0 | - | 0.0 |
| 225 | insulation minimum outside diameter (neglects pipe wall) | $D_{\min_insul} = 2 * \lambda / \ln(D_{\text{insul}} / D)$ | mm | 104.4 | 80.6 | 54.0 | 26.2 | 23.0 | 23.0 | 11.5 | - | 67.8 |
| 226 | insulation minimum thickness (no margin) | tmin_insul | mm | 2.2 | 2.8 | 2.0 | 1.6 | 0.0 | 0.0 | 0.0 | - | 3.1 |
| 227 | insulation design thickness | $t_{\text{insul}} = t_{\text{design_factor}} * t_{\min_insul}$ | mm | 4.4 | 5.6 | 4.0 | 3.2 | 0.0 | 0.0 | 0.0 | - | 6.2 |
| 228 | pipe + insulation outer diameter (pipe wall neglected) | D_total_no_wall | mm | 108.8 | 86.1 | 58.0 | 29.4 | 23.0 | 23.0 | 11.5 | - | 73.9 |

Insulation thickness at the entrance pipes is much reduced

Humidity management strategy

- Supply air quality: water content
 - \leq Class 3 (i.e. -20°C pressure dew point)
 - per ISO 8573-1:2010
- Insulate exterior cold pipes
 - from air supply plant to ePIC: efficiency, good housekeeping
 - from exterior to SVT: prevent condensation on detectors
 - once inside SVT we have guarantees on air dryness
- Interlock if WAH HVAC fails and/or exterior dew point above insulation design value (e.g. 13°C TBC)
- If air flow shuts down while interior structures are cold...
 - must prevent significant backflow into system from exterior
 - i.e. provide high impedance (not an airtight seal) against moisture effusion
 - flapper valves on exhaust duct outlets
 - closeouts elsewhere
- Air supply diverter valve
 - vents air to bypass outlet if fault condition
 - during startup no air flow to SVT until guaranteed dry
 - supply plant can be tested / operated / fixed without running air to SVT

Air quality strategy

- ISO 8573-1:2010 defines compressed air purity classes
- Supply air quality
 - solid particulate: Class 1
 - total oil: Class 1
 - water: \leq Class 3
- Air supply diverter valve
 - vent supply air to bypass outlet for startup, air quality test, etc
- Additional air filters at manifolds just outside ePIC
 - extra line of defense

| CLASS | SOLID/DIRT Particle size | | | WATER @7 bar/100 psi Pressure Dewpoint | | OIL Including vapor |
|-------|--|-----------------------|-----------------------|--|--------------------|------------------------|
| | 0.1-0.5 μm | 0.5-1.0 μm | 1.0-5.0 μm | | | |
| | Maximum number of particles per m^3 | | | $^{\circ}\text{C}$ | $^{\circ}\text{F}$ | mg/m^3 |
| 0 | As specified by the equipment user or supplier | | | | | |
| 1 | $\leq 20\,000$ | ≤ 400 | ≤ 10 | -70 | -94 | ≤ 0.01 |
| 2 | $\leq 400\,000$ | $\leq 6\,000$ | ≤ 100 | -40 | -40 | ≤ 0.1 |
| 3 | - | $\leq 90\,000$ | $\leq 1\,000$ | -20 | -4 | ≤ 1 |
| 4 | - | - | $\leq 10\,000$ | +3 | +38 | ≤ 5 |
| 5 | - | - | $\leq 100\,000$ | +7 | +45 | > 5 |
| 6 | - | - | - | +10 | +50 | - |

Source: [Atlas Copco](#)

System calcs + humidity management + air quality + control considerations → detailed specs on air supply plant

| A | B | C | D | E | F | G | H | I | |
|--|-------------|--|-----------------|-----------------------------|-------------|------------|-------------|---|---|
| ePIC SVT Air Supply Plant - Requirements | | | | | | | | | |
| | | | | | | | | | |
| Contact | | | | Color key: | | | | | |
| Joe Silber <jhsilber@lbl.gov> | | | | INPUT | | | | | |
| Lawrence Berkeley National Laboratory | | | | CALCULATED | | | | | |
| | | | | LINKED | | | | | |
| Version history | | | | | | | | | |
| v1 - 2025-11-11 - JHS - initial version | | | | | | | | | |
| v2 - 2025-11-19 - JHS - wider T_stability, diverter, moisture in terms of DP's, possible enclosure, add'l comments | | | | | | | | | |
| | | | | | | | | | |
| Abstract | | | | | | | | | |
| The Silicon Vertex Tracker (SVT) is a key subsystem of the Electron-Proton/Ion Collider (ePIC) detector. It will probe the smallest internal building blocks of visible matter -- quarks and gluons -- and help us understand the underlying laws that govern the strongest force in nature. | | | | | | | | | |
| The SVT is composed of thousands of custom silicon sensors. They will be cooled by a steady supply of cleaned, conditioned, cooled air. This specification is for the plant which will generate that cooling air. This specification does not include the transmission of that air to the SVT. | | | | | | | | | |
| | | | | | | | | | |
| ID | Category | Description | Name | Value (SI) | Units (SI) | Value (US) | Units (US) | Comments | |
| 00 | process air | temperature - nominal | T_nom | 37.4 | °C | 97.4 | °F | Possible future relaxation of T_nom to +12°C (TBD) | |
| 01 | output air | temperature - adjustment range - min | T_min | -5 | °C | 23.0 | °F | Possible future relaxation of T_min to +7°C (TBD) | |
| 02 | output air | temperature - adjustment range - max | T_max | 38 | °C | 86.0 | °F | | |
| 03 | output air | temperature - stability about setpoint | T_stability | ±2 | °C | ±3.6 | °F | | |
| | | | | | | | | | |
| 04 | output air | pressure dew point - max allowable | PDP_max_allow | -10 | °C | 14.0 | °F | Pressure dew point shall never exceed this value when output stream is flowing through the process outlet. Possible future relaxation of PDP_max_allow to +3°C (TBD). | |
| 05 | output air | pressure dew point - stability | PDP_stability | ±2 | °C | ±3.6 | °F | | |
| Pressure dew point shall be settable within a range defined by the AQ_water class (at low end) to PDP_max_allow (at high end). | | | | | | | | | |
| 06 | output air | pressure dew point - setpoint adjustment | PDP_setpoint | | | | | | |
| 07 | output air | pressure - nominal | P_nom | 0.44 | bar (gauge) | 6.4 | psi (gauge) | | |
| 08 | output air | pressure - adjustment range - min | P_min | 0.03 | bar (gauge) | 0.4 | psi (gauge) | | |
| 09 | output air | pressure - adjustment range - max | P_max | 0.75 | bar (gauge) | 10.9 | psi (gauge) | | |
| 10 | output air | pressure - stability about setpoint | P_stability | ±0.02 | bar (gauge) | ±0.29 | psi (gauge) | | |
| 11 | output air | mass flow rate - nominal | m_nom | 1.0 | kg/s | 132 | lbm/min | | |
| 12 | output air | mass flow rate - adjustment range - min | m_min | 0.1 | kg/s | 13 | lbm/min | | |
| 13 | output air | mass flow rate - adjustment range - max | m_max | 1.5 | kg/s | 198 | lbm/min | | |
| 14 | output air | density - nominal | ρ_nom | 1.82 | kg/m³ | 0.11 | lbm/ft³ | at P_nom, T_nom | |
| 15 | output air | density - min | ρ_min | 1.18 | kg/m³ | 0.07 | lbm/ft³ | at P_min, T_max | |
| 16 | output air | density - max | ρ_max | 2.27 | kg/m³ | 0.14 | lbm/ft³ | at P_max, T_min | |
| 17 | output air | volumetric flow rate - nominal | V_nom | 0.55 | m³/s | 1166 | ft³/min | at P_nom, T_nom | |
| 18 | output air | volumetric flow rate - min | V_min | 0.08 | m³/s | 179 | ft³/min | at P_min, T_max | |
| 19 | output air | volumetric flow rate - max | V_max | 0.66 | m³/s | 1398 | ft³/min | at P_max, T_min | |
| 20 | output air | air quality - solid particulate | AQ_particulates | Class 1 per ISO 8573-1:2010 | | | | | |
| 21 | output air | air quality - total oil | AQ_oil | Class 1 per ISO 8573-1:2010 | | | | | Oil-free compression or high-end filtration is critical to prevent oil contamination. |

| A | B | C | D | E | F | G | H | I |
|----|----|-------------|--|---|---|---------|-----------|-----|
| 38 | 22 | output air | air quality - humidity / water | AQ_water | Class 2 PDP = -40°C, Class 3 = -20°C, might consider Class 4 (PDP=+3°C) if significant cost savings and if T_min could be increased to +10°C (TBD) | | | |
| 39 | | | | Class 3 per ISO 8573-1:2010 | | | | |
| 39 | | | | Plant shall have an integrated 3-way diverter valve on the output stream. Outlets are to "process" (goes to SVT instrument) and "bypass" (exhaust). Fail-safe state (e.g. upon loss of power) shall be to the bypass outlet. | | | | |
| 40 | 23 | output air | output diverter | diverter_valve | 100 | mm | 4 | in |
| 40 | 24 | facility | hose inner diameter - process air | Dh_process | TBD | mm | TBD | in |
| 41 | 25 | facility | hose inner diameter - bypass air | Dh_bypass | TBD | mm | TBD | in |
| 42 | 26 | facility | hose fitting type - process air | fitting_process | TBD | - | - | - |
| 43 | 27 | facility | hose fitting type - bypass air | fitting_bypass | TBD | - | - | - |
| 44 | 28 | facility | electrical - plug form | e_plug | TBD | - | - | - |
| 45 | 29 | facility | supply voltage | V_supply | TBD | - | - | - |
| 46 | 30 | facility | supply frequency | f_supply | 60 | Hz | - | - |
| 47 | 31 | facility | heat rejection - coolant | coolant | TBD | - | - | - |
| 48 | 32 | facility | heat rejection - coolant temperature | Tc | TBD | °C | K | ° |
| 49 | 33 | facility | heat rejection - coolant flow rate limit | Vc | TBD | L/min | ? | ° |
| 50 | 34 | facility | heat rejection - coolant pressure | Pc | TBD | ? | ? | ° |
| 51 | 35 | environment | ambient temperature during operation - avg | T_amb_avg | 23 | °C | 73.4 | °F |
| 52 | 36 | environment | ambient temperature during operation - min | T_amb_min | 18 | °C | 64.4 | °F |
| 53 | 37 | environment | ambient temperature during operation - max | T_amb_max | 32 | °C | 89.6 | °F |
| 54 | 38 | environment | ambient dewpoint during operation - avg | DP_amb_avg | 5.2 | °C | 41.4 | °F |
| 55 | 39 | environment | ambient dewpoint during operation - max | DP_amb_max | 22.1 | °C | 71.8 | °F |
| 56 | | | | System shall have a process_fault condition, based on measured state of the output air. The state is logically TRUE when any of the key parameters (temperature, pressure, or pressure dew point) falls outside either its user-configured allowable range or the limit values listed here (whichever is more restrictive). | | | | |
| 56 | | | | System shall automatically direct output air to the bypass outlet during startup, shutdown, or process_fault state. | | | | |
| 57 | 40 | control | fault condition on process air | process_fault | Plant shall have a local user-interface panel by which it can be operated. | | | |
| 57 | 41 | control | output diverter control | diverter_ctrl | Plant shall have an API allowing customer to integrate it into our facility's control system, for configuring, monitoring, and real-time control. | | | |
| 58 | 42 | control | control interface - local | ctrl_local | Emergency shut-off shall be readily achievable by pressing an easily-identifiable hardware button, by any person physically stationed near the plant. | | | |
| 59 | 43 | control | control interface - remote | ctrl_remote | Emergency shut-off shall be readily achievable by a simple electrical interlock signal. | | | |
| 60 | 44 | control | emergency shut-off - local | shutoff_local | | | | |
| 61 | 45 | control | emergency shut-off - remote | shutoff_remote | 99.5 | % | TBD | in |
| 62 | 46 | maintenance | uptime during normal operations | uptime | 47 | package | max width | TBD |
| 63 | 47 | package | max width | W_max | TBD | m | TBD | in |
| 64 | 48 | package | max length | L_max | TBD | m | TBD | in |
| 65 | 49 | package | max height | H_max | TBD | m | TBD | in |
| 66 | 50 | package | max weight | M_max | TBD | kg | TBD | lbm |
| 67 | 51 | package | enclosure | enclosure | TBD, possibly include load component (e.g. compressor) for moderate sound dampening | | | |

Link: [ePIC SVT air supply plant reqts - v2.xlsx](#)